

26,27 and the facing surfaces 16 of anode 15, as well as between the aluminium canal 40' and the facing flattened part 17 of the anode 15 which will wear in such a way as to conform to the opposing surfaces (26,27 and the flat top of canal 40'). Moreover, the inclination of anode surfaces 16 assists in release of the anodically-formed gases. Alternatively, it is possible to operate in a drained configuration without an aluminium canal 40', or with a narrow and shallow canal of aluminium.

FIG. 5 shows a cell of similar design, where the same elements are designated by the same references, but which includes dimensionally stable anodes 18 in a "roof" configuration straddling the tops of the adjacent carbon cathode blocks 10 which also have alternately arranged inclined surfaces 26,27 coated with an aluminium-wettable refractory coating 35.

The anode plates 18 are made of or coated with any suitable non-consumable or substantially non-consumable, electronically-conductive material resistant to the electrolyte and to the anode product of electrolysis, which is normally oxygen. For example, the plates may have a metal, alloy or cermet substrate which is protected in use by a cerium-oxyfluoride-based protective coating produced and/or maintained by maintaining a concentration of cerium in the electrolyte, as described in U.S. Pat. No. 4,614,569.

The anodes 18 preferably are substantially non-consumable refractory materials resistant to the oxygen produced and the other gases, vapors and fumes, present in the cell, and resistant to chemical attack by the electrolyte.

The cell of FIG. 5 also operates as a drained cathode cell, wherein the aluminium produced on the inclined cathode surfaces 26 and 27 coated with an aluminium-wettable refractory coating 35 flows down to the bottom of these inclined surfaces where it is collected as an aluminium canal 40' in a groove 28' which is generally U-shaped in cross-section. As before, the cathode surfaces 26,27 are inclined in the longitudinal direction of the cell in order to permanently drain the product aluminium, at a rate to keep the level of the aluminium canal 40' stable. In this drained configuration, the grooves 28' are thus filled with the molten aluminium forming canal 40'. Electrolysis takes place between the aluminium-wetted cathode surfaces 26,27 and the facing surfaces of the dimensionally-stable anodes 18. The inclination of anodes 18 assists in release of the anodically-formed gases through a central opening 19 and this can be further assisted if needed by providing ridges on the anodes 18 or making the anodes foraminated.

FIG. 6 shows part of another cell according to the invention similar to the cell shown in FIG. 2. Instead of having a wavy channeled surface, the blocks 10 have bevelled upper side edges 20 and may be bevelled also along their top end edges, as indicated in dotted lined at 29. The bevelled side edges 20 of the adjacent blocks form V or U-shaped channels running along the blocks 10, there being a similar V or U-shaped channel formed between the bevelled a similar the sidemost block 10 to and the adjacent mass of ramming paste 34.

In FIG. 6, the adjacent blocks 10 are shown as being bonded together by a glue 14', so there is essentially no gap between them. As shown, the aluminium-wettable refractory coating 35 covers the entire upper surfaces of blocks 10 with bevels 20 and 29, the glued joints 14', and also extends over the adjacent mass of ramming paste 34.

The purpose of the cross-bevels 29 in the top end edges of the blocks 10 is to form a cross-channel perpendicular to the parallel channels formed by the V or U-shaped grooves

between bevels 20, for draining off the product aluminium to maintain canals 40' of aluminium in the V or U-shaped grooves at a constant level. Such cross-channels can be formed in one or both ends of the blocks and, if required, one or more intermediate cross channels can be formed by machining grooves across the blocks 10, intersecting with the V or U-shaped grooves formed by bevels 20.

These cross-channels are connected to a reservoir of molten aluminium, possibly with a weir in order to set the level of the aluminium canals 40'. Operation is possible with a fluctuating level of the aluminium canals 40' or with a steady level.

The present invention has been described with respect to preferred embodiments. Modifications and alterations will occur to others upon the reading and understanding of the specification. It is intended that all such modifications and alterations be included insofar as they come within the scope of the invention as claimed and equivalents thereof.

What is claimed is:

1. An electrolytic cell for the electrowinning of aluminium from alumina dissolved in a fluoride-based molten electrolyte, having a series of anodes facing a cathode cell bottom, the cathode cell bottom comprising a series of juxtaposed cathode blocks each having a sloped drained top cathode surface down which a layer of produced molten aluminium is continuously drained when the cathode block is in use to electrowin aluminium, the top surfaces of several cathode blocks placed laterally side-by-side forming a series of V-shaped sloped cathode surfaces, each cathode block further comprising a cut-out along the lower edge of its sloped top surface, so that two cathode blocks placed side-by-side and forming a V-shaped cathode surface have a recessed groove formed between them by juxtaposition of their respective cut-outs, said recessed groove being located along and below the bottom of the V-shaped sloped cathode surface, said groove during cell operation collecting and evacuating the molten aluminium drained from the bottom of the sloped V-shaped cathode surfaces.

2. The electrolytic cell of claim 1, wherein the cell bottom is made of a series of carbon cathode blocks, each having a sloped top surface, a plurality of side surfaces and a bottom surface, the cathode blocks being connected side-by-side, transverse to the cell, said blocks being further provided with conductive bars for the delivery of current, said conductive bars being generally parallel to one another and transverse to the cell.

3. The electrolytic cell of claim 2, wherein at least some of the recessed grooves are formed by cut-outs along the edges of the cathode blocks.

4. The electrolytic cell of claim 2, wherein the sloping surfaces of the cathode blocks making up the cell bottom are treated to reduce sodium penetration.

5. The electrolytic cell of claim 4, wherein the sloping surfaces of the cathode blocks making up the cell bottom are coated with a layer which reduces sodium penetration.

6. The electrolytic cell of claim 2, wherein the sloping surfaces of the cathode blocks making up the cathode cell bottom are coated with a layer which, prior to or in use, becomes harder than the carbon cathode block.

7. The electrolytic cell of claim 2, wherein the cathode blocks remain dimensionally stable during electrolysis.

8. The electrolytic cell of claim 2, wherein the cathode blocks are made resistant to chemical and mechanical attack.

9. The electrolytic cell of claim 1, wherein the sloped cathode surfaces of the cathode cell bottom are coated with a layer of aluminium-wettable refractory material.

10. The electrolytic cell of claim 1, wherein the molten aluminium is at a constant level within the recessed grooves.

11. The electrolytic cell of claim 1, wherein the sloped cathode surfaces further comprise at least one cross channel which intersects with the parallel recessed grooves, said cross channel extending in the longitudinal direction of the cell.

12. The electrolytic cell of claim 11, wherein the cell bottom is sloping longitudinally and wherein the cross channels run down the sloping cell bottom.

13. The electrolytic cell of claim 1, wherein the recessed grooves have a U-shaped cross-section.

14. The electrolytic cell of claim 1, wherein the recessed grooves have a rectangular cross-section.

15. The electrolytic cell of claim 1, wherein the recessed grooves have a trapezoidal cross-section.

16. The electrolytic cell of claim 1, wherein the recessed grooves have a V-shaped cross-section.

17. The electrolytic cell of claim 1, wherein the recessed grooves have a curved or rounded cross-section.

18. The electrolytic cell of claim 1, wherein the recessed grooves have an asymmetric cross-section.

19. The electrolytic cell of claim 11, wherein the cell bottom comprises a plurality of pairs of two longitudinally sloping parts and the cross channels run down these sloping parts, there being at the intersection of the two sloping parts a collecting recessed groove, said cross channel leading to an aluminium reservoir.

20. The electrolytic cell of claim 1, wherein the recessed grooves extend transversely with respect to the cell and lead into at least one cross channel arranged longitudinally with respect to the cell for collecting the molten aluminium.

21. A method of manufacturing the cathode bottom of an electrolytic cell for the electrowinning of aluminium from alumina dissolved in a fluoride-based molten electrolyte, said cell having a series of anodes facing a cathode cell bottom, the cathode cell bottom comprising a series of juxtaposed cathode blocks each having a sloped drained top cathode surface down which a layer of produced molten aluminium is continuously drained when the cathode block is in use to electrowin aluminium, the top surfaces of several cathode blocks placed laterally side-by-side forming a series of V-shaped sloped cathode surfaces, the method comprising:

- a) before or after assembling the cathode blocks in a cell providing a sloping cathode top surface on each cathode block; and
- b) further providing a cut-out along the bottom of each sloping cathode top surface so that two cathode blocks placed side by side in the cell form a V-shaped top surface with a recessed groove formed between them,

said recessed groove formed by the juxtaposition of the respective cut-outs of the cathode blocks, said recessed groove being located along and below the bottom of the V-shaped sloped cathode surface, and said groove during cell operation collecting and evacuating the molten aluminium drained from the bottom of the sloped V-shaped cathode surfaces.

22. The method of claim 21, wherein the recessed grooves and/or sloping sections are machined in the top of the cathode blocks.

23. The method of claim 21, comprising the further step of treating the cathode blocks to make them resistant to chemical and mechanical attack.

24. The method of claim 21, wherein before start up of the cell for producing aluminium, the cell bottom is treated to harden the top surfaces of the cathode blocks and to render the top surfaces wettable by molten aluminium, thereby rendering the cathode blocks dimensionally stable during electrolysis.

25. A method of producing aluminium in a cell for the electrowinning of aluminium from alumina dissolved in a fluoride-based molten electrolyte, said cell having a series of anodes facing a cathode cell bottom, the cathode cell bottom comprising a series of juxtaposed cathode blocks each having a sloped drained top cathode surface down which a layer of produced molten aluminium is continuously drained when the cathode block is in use to electrowin aluminium, the top surfaces of several cathode blocks placed laterally side-by-side forming a series of V-shaped sloped cathode surfaces, each cathode block further comprising a cut-out along the lower edge of its sloped top surface, so that two cathode blocks placed side-by-side and forming a V-shaped cathode surface have a recessed groove formed between them by juxtaposition of their respective cut-outs, said recessed groove being located along and below the bottom of the V-shaped sloped cathode surface, the method comprising:

- a) passing an ionic current between the cathode bottom and facing anodes to electrolyze dissolved alumina;
- b) thereby producing gas on the anodes and aluminium on the drained cathode surfaces; and
- c) allowing the produced molten aluminium to drain down the cathode surfaces into the collection and evacuation grooves located along the bottom of the V-shaped sloped cathode surfaces and extending below the sloped cathode surfaces.